

Model-Based Optimization and Control of Subsurface Flow in Oil Reservoirs

Paul Van den Hof

Eindhoven University of Technology, The Netherlands

with: Jan Dirk Jansen and Arnold Heemink, Delft Univ. Techn.

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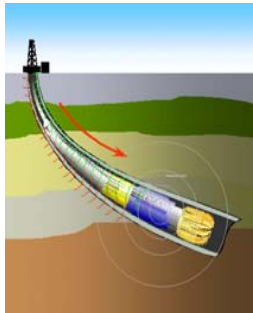
Upstream oil industry



production



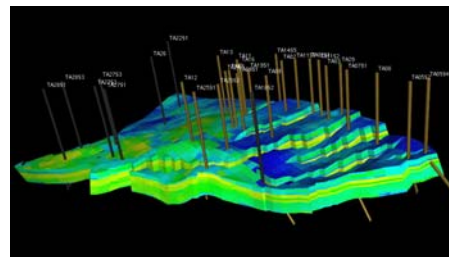
seismic
imaging



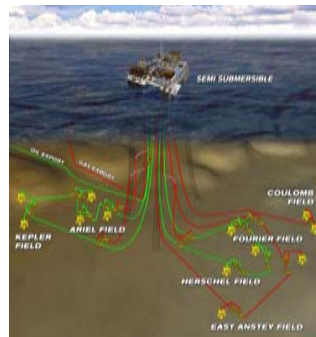
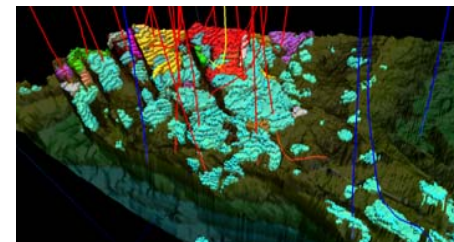
drilling



reservoir modeling



geological
modeling

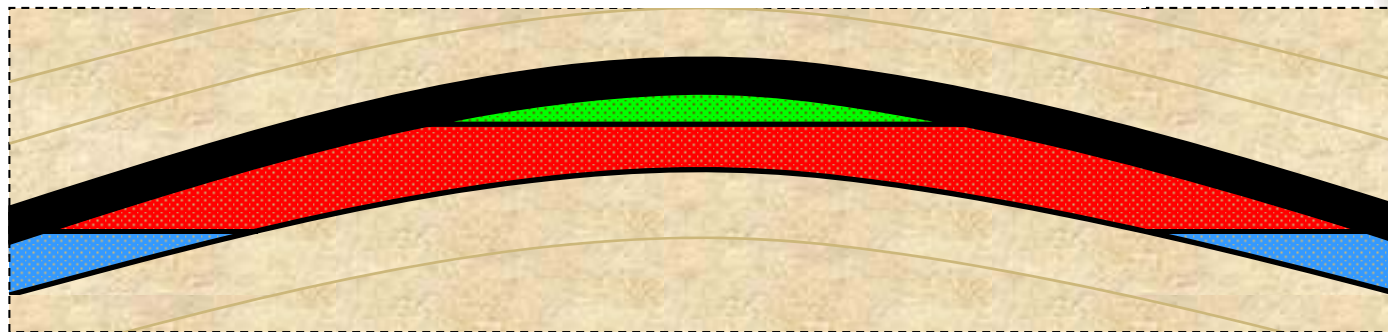


Upstream oil industry characteristics

- **Capital intensive:** well: 1-100· 10⁶ US\$, field: 0.1-10· 10⁹ US\$
- **Uncertainty:** geology, oil price, limited data
- **Stretched in time scales:**
 - production operations: day – weeks
 - field development – years
 - reservoir management: 10s of years
- **Slow in response**
- **Many disciplines involved:** geology, geophysics, reservoir engineering, production, drilling
- **Remote**
- **New technology:** horizontal drilling, multi-laterals, time lapse seismics, smart fields

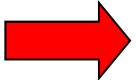
Oil Production

- Production from Oil Reservoirs
 - Porous rock with oil in pores
 - Geological structure heterogeneous
 - Very different rock properties within reservoir
 - $10^1 - 10^4$ km² in size
 - 10^3 m – 10^4 m underground
 - Difficult locations



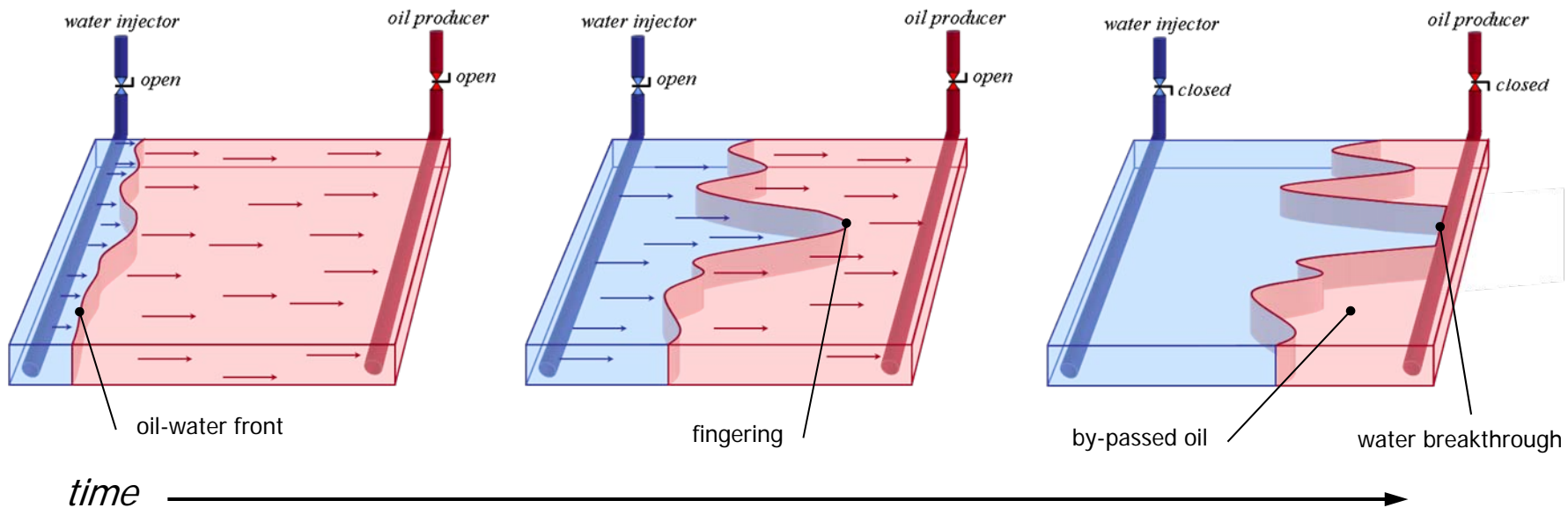
- cap rock
- water bearing reservoir rock
- non- reservoir rock
- oil bearing reservoir rock
- gas bearing reservoir rock

Oil production mechanisms

- Primary recovery – natural flow
(depletion drive, 5-15% recovery)
-  Secondary recovery – injection of water or gas to maintain reservoir pressure and displace oil actively
(water flooding, gas flooding, 20-70% recovery)
- Tertiary recovery – injection of steam or chemicals (polymers, surfactants) to change the in-situ physical properties (e.g. viscosity, surface tension)
(steam flooding, polymer flooding, 20-90% recovery)

Waterflooding

- Involves the injection of water through the use of **injection** wells
- Goal is to increase reservoir pressure and displace oil by water
- Production is terminated when ratio between produced oil and water is no longer **economically** viable



Waterflooding

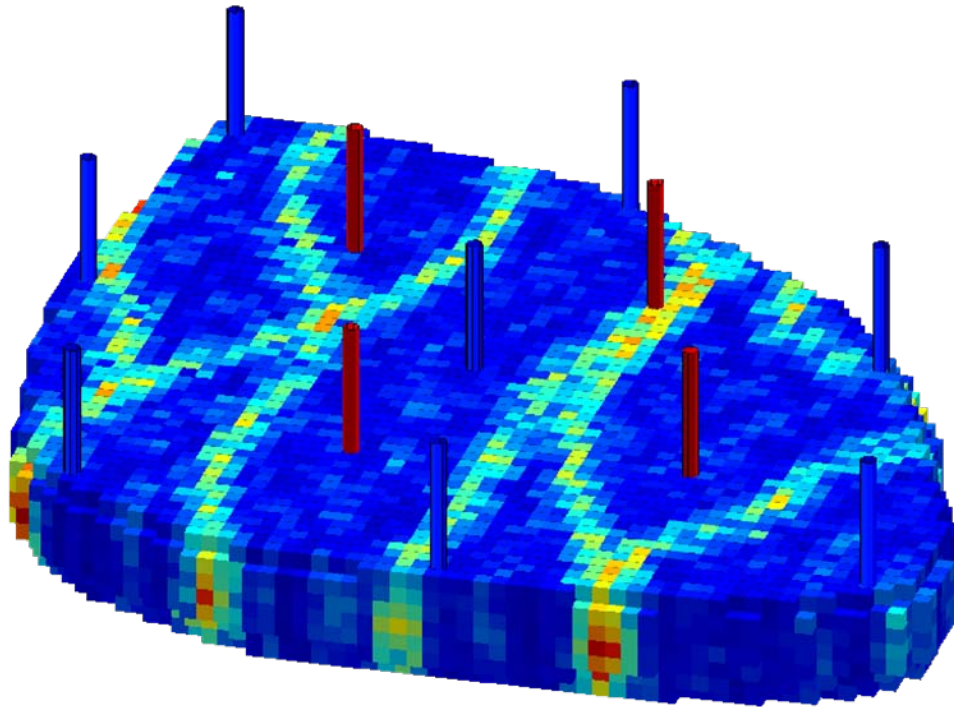
Waterflooding (WF)

Essentially a batch process

- Life time in the order of decades
- Potential to recover **20-70%** of the oil

Limited in practice by lack of operational strategy

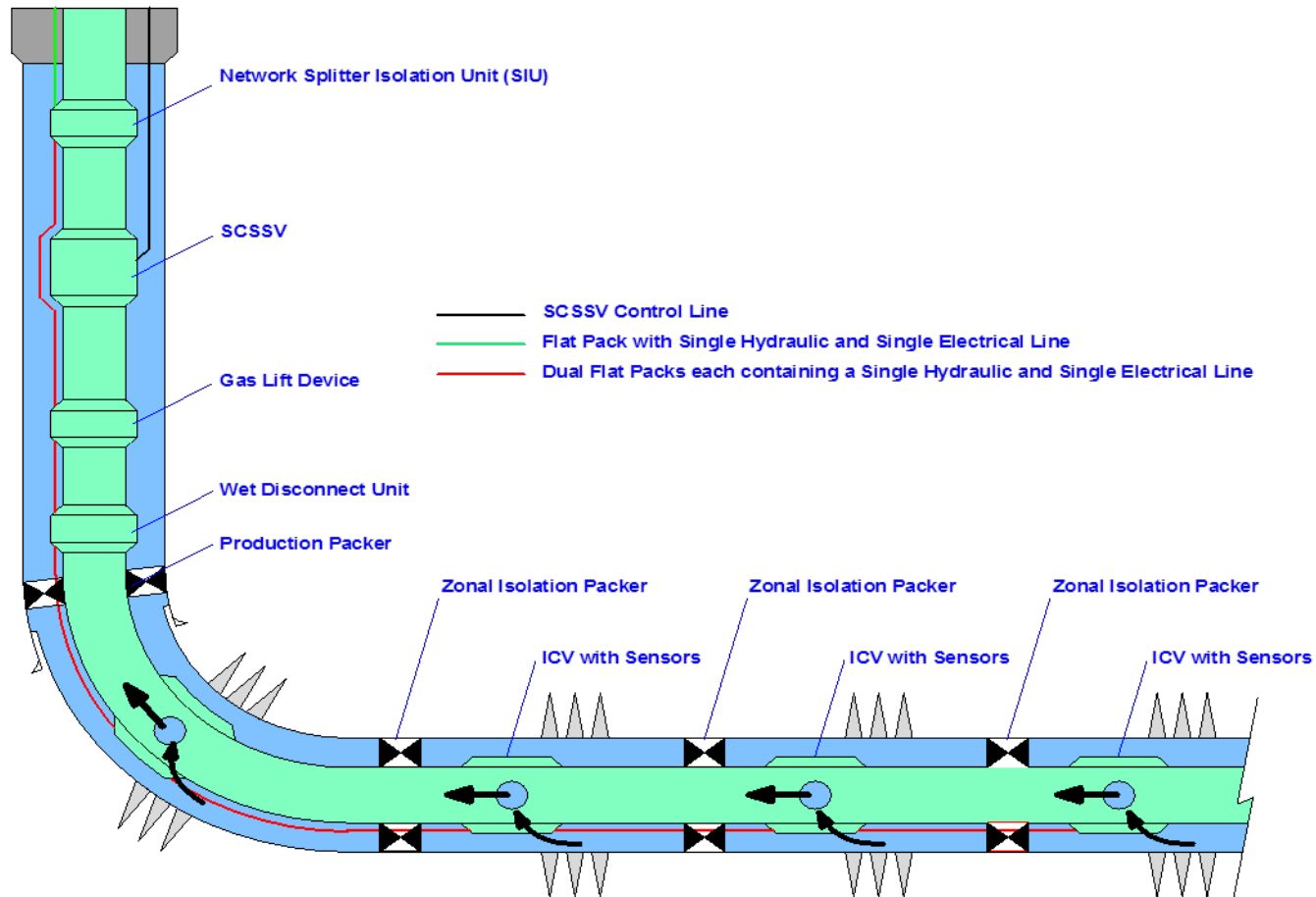
Reservoir characteristics



(Gijs van Essen et al., CAA 2006)

- 3D
- heterogeneity of reservoir
- flow dynamics determined by geological structure (permeability)

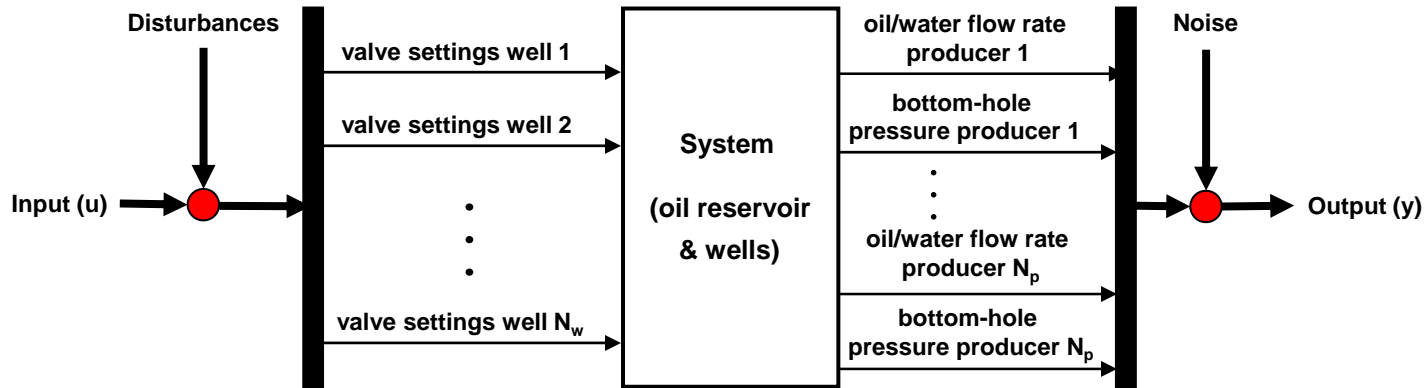
Smart well with inflow control valves



- Smart wells allow control over (distributed) local valve settings in injectors and producers, and local measurements.

The Objective

- **Inputs:** control valve settings of the wells (injectors and producers)
 - Smart wells: multiple (subsurface) valves
- **Outputs:** (fractional) flow rates and/or bottomhole pressures
 - Smart wells: multiple (subsurface) measurement devices



Objective: Economic operational strategy that optimizes performance (life cycle)

Contents

- Introduction
- **Closed-loop reservoir management**
- Current limitations and challenges

- Robust optimization
- Balancing long-term and short-term objectives (hierarchical)
- Parameter estimation
- Time-scale separation – 2-level approach
- Control-relevant models

- Discussion

The models

Mass balance:

$$\nabla \cdot (\rho_i u_i) + \frac{\partial}{\partial t}(\phi \rho_i S_i) = 0 \quad i = \{o, w\}$$

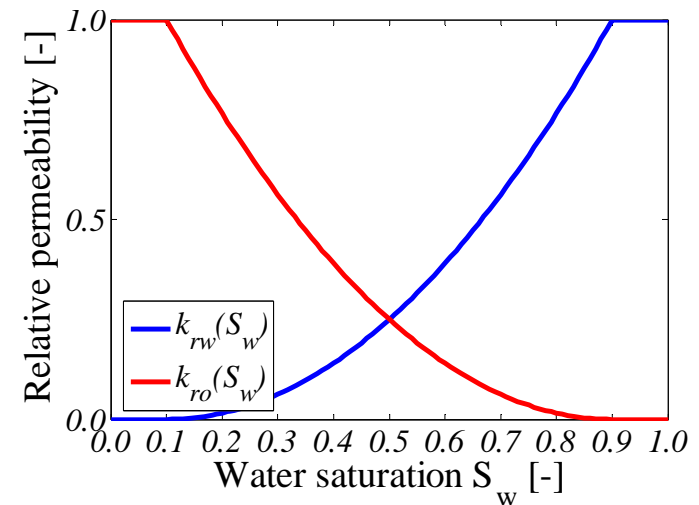
Momentum (Darcy's law):

$$u_i = -k \frac{k_{ri}}{\mu_i} \nabla p_i \quad i = \{o, w\}$$

Variables: p_o, p_w, S_o, S_w

Saturations satisfy: $S_o + S_w = 1$

Simplifying assumptions, a.o.: $p_o = p_w$



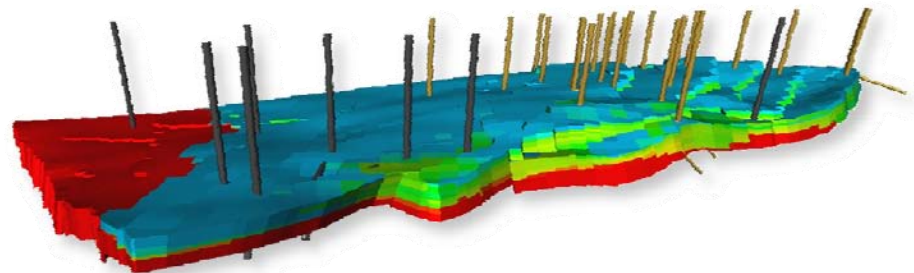
Discretization in space and time

After discretization in space (and time):

$$\begin{aligned} g(x_{k+1}, x_k, u_k, \theta) &= 0 & \dim(x) &\approx 10^4 - 10^6 \\ y_k &= h(x_k) & y_k^T &= [p_{well}^T \ q_{well,o}^T \ q_{well,w}^T] \\ x_k^T &= [p_o^T \ S_w^T] \end{aligned}$$

and θ typically the permeabilities in each grid block

- Models are large-scale
- Nonlinear
- Long simulation time
- Typically used off-line
- Actually a batch-type process



Model-based Life-Cycle Optimization

Net present value (NPV):

$$J_K = \sum_{k=1}^K \left[\frac{r_o \cdot q_{o,k}(y_k) - r_w \cdot q_{w,k}(y_k) - r_{inj} \cdot q_{inj,k}(u_k)}{(1+b)^{\frac{t_k}{\tau_t}}} \cdot \Delta t_k \right]$$

Optimization problem:

$$\begin{aligned} & \max_{\mathbf{u} \in Q} J_K(\mathbf{u}, x_0), \\ & \text{subject to } \mathbf{g}(\mathbf{u}, \mathbf{x}) = 0, \quad x_0 = \bar{x}_0, \\ & \text{and } \mathbf{c}(\mathbf{x}, \mathbf{u}) \leq 0, \quad \mathbf{d}(\mathbf{x}, \mathbf{u}) = 0 \end{aligned}$$

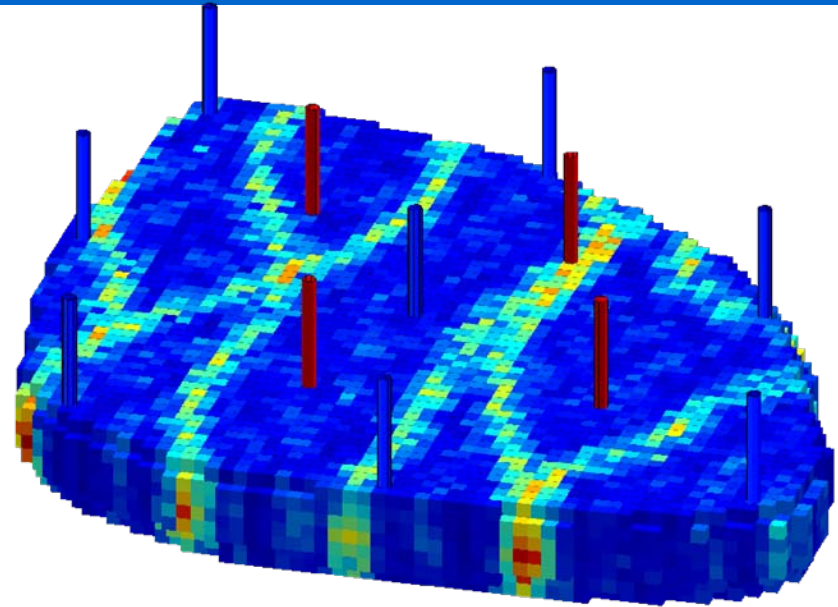
Non-convex optimization, solved by gradient-based method:
Adjoint-variables calculation through backward integration of
the related (Hamiltonian based adjoint) equation.

(feasible for systems of this size)

[Ramirez, 1987; Brouwer &
Jansen, SPE J, 2004]

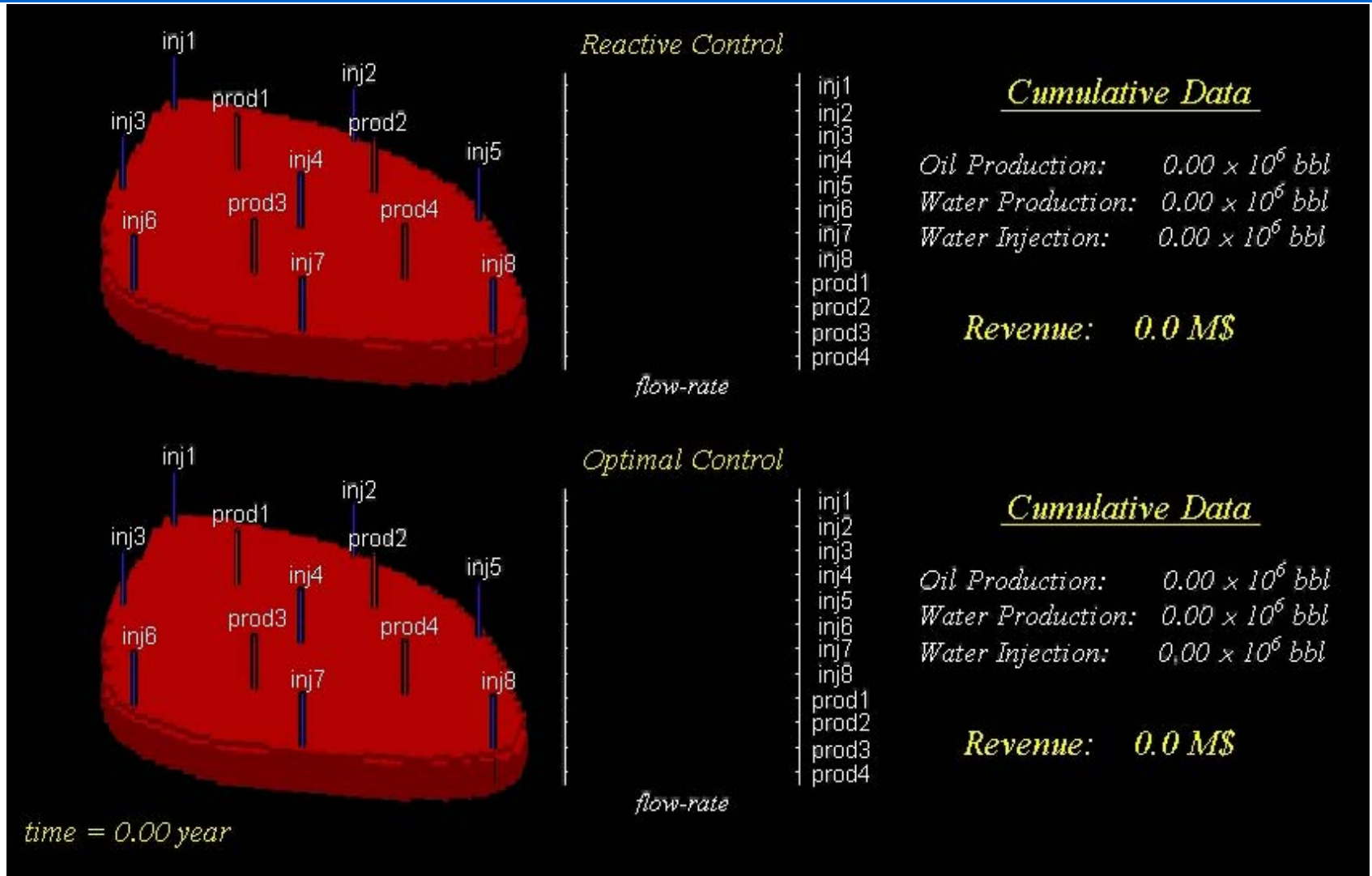
12-well example

- 3D reservoir
- 8 injection / 4 production wells
- Period of 10 years
- High-permeability channels
- 18.553 grid blocks
- Minimum rate of 0.1 *stb/d*
- Maximum rate of 400 *stb/d*
- No discount factor
- $r_o = 20$ *\$/stb*, $r_w = 3$ *\$/stb* and $r_i = 1$ *\$/stb*
- Optimization of economic revenues (NPV)
- Model-based optimal control with a known model

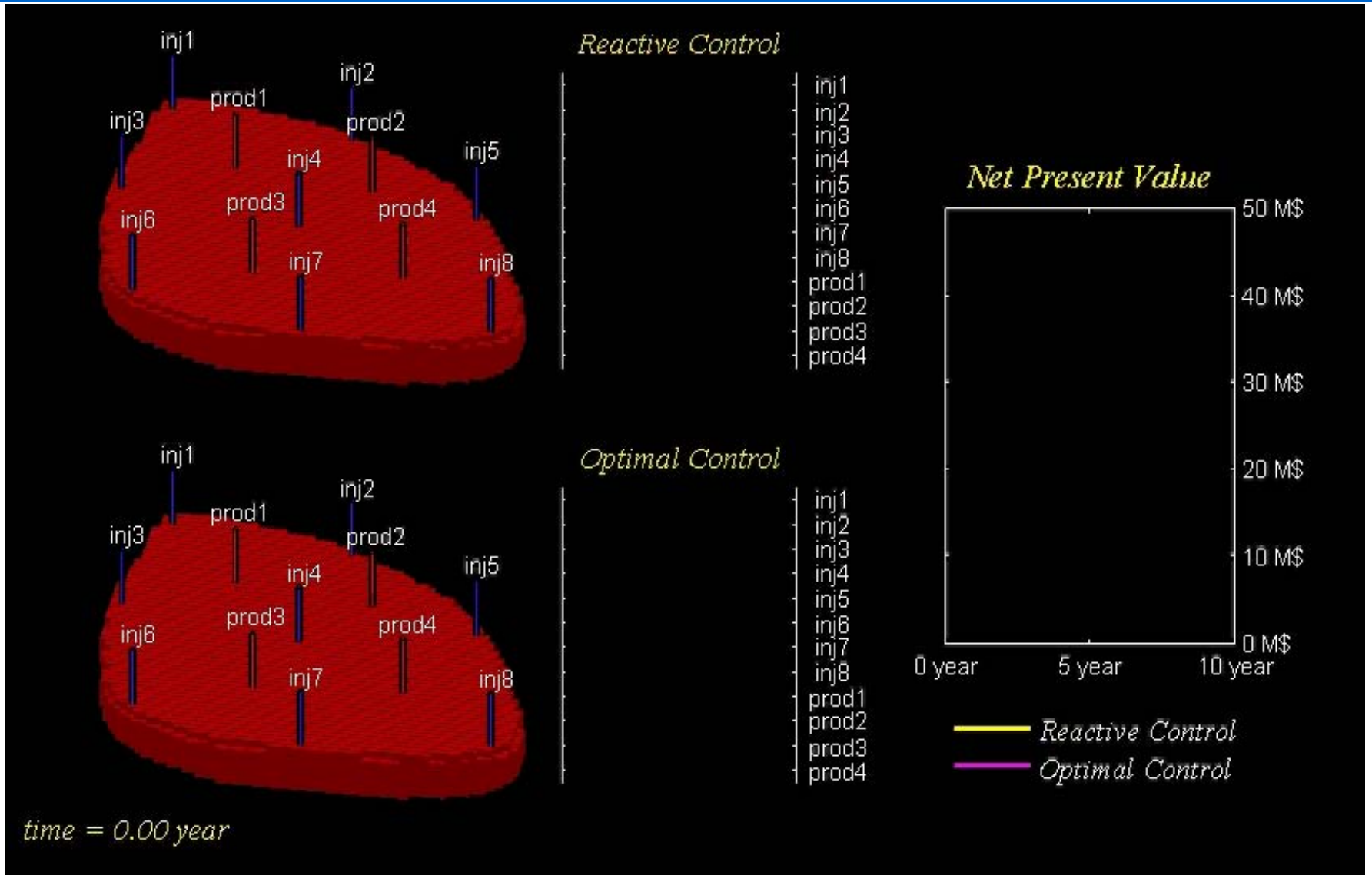


(Gijs van Essen et al.,
CAA 2006)

Reactive versus optimal control



Reactive versus optimal control



Closed-loop Reservoir Management

- Moving from (batch-wise) open-loop optimization to **on-line closed-loop control**
 - State estimator
 - Optimized plant input through NMPC in receding/shrinking horizon
 - No trajectory following but dynamic RTO

But how about the model?

Closed-loop Reservoir Management

Obtaining a model

- **First-principle models** (geology) are highly uncertain
- Opportunities for **identification** are limited (nonlinear behaviour dependent on front-location, single batch process, experimental limitations)
- Option: **estimate** physical parameters (permeabilities) in first principles model; starting with initial guess

Closed-loop Reservoir Management

Several options for nonlinear state and parameter estimation:

Available from oceanographic domain:

Ensemble Kalman filter (EnKF) (Evensen, 2006)

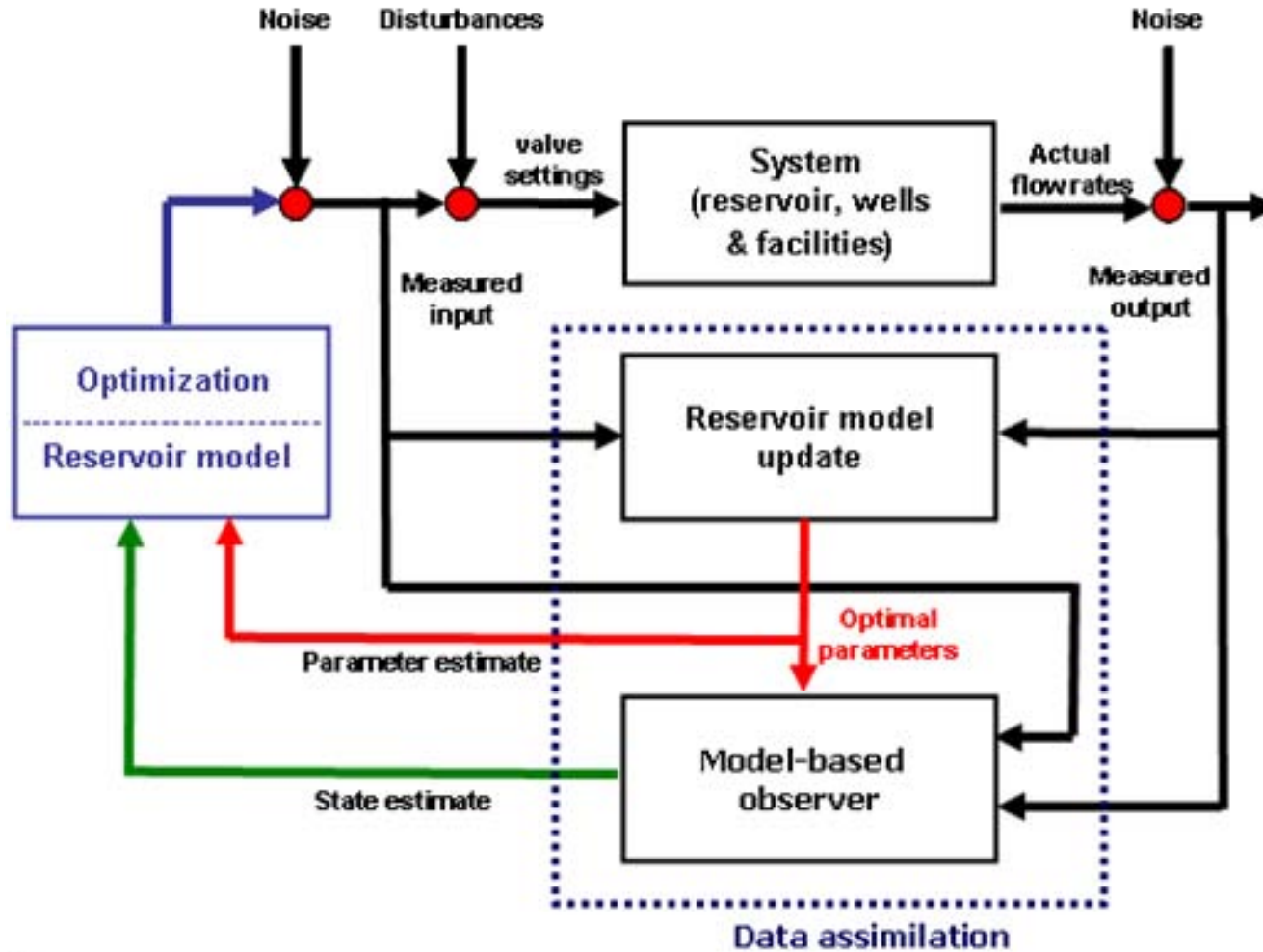
- Kalman type estimator, with analytical error propagation replaced by Monte Carlo approach (error cov. matrix determined by processing ensemble of model realizations)
- Ability to handle model uncertainty (in some sense)
- In reservoir engineering used for estimation of states **and parameters** (history matching)

Note: # parameters = # states

Ensemble Kalman Filter

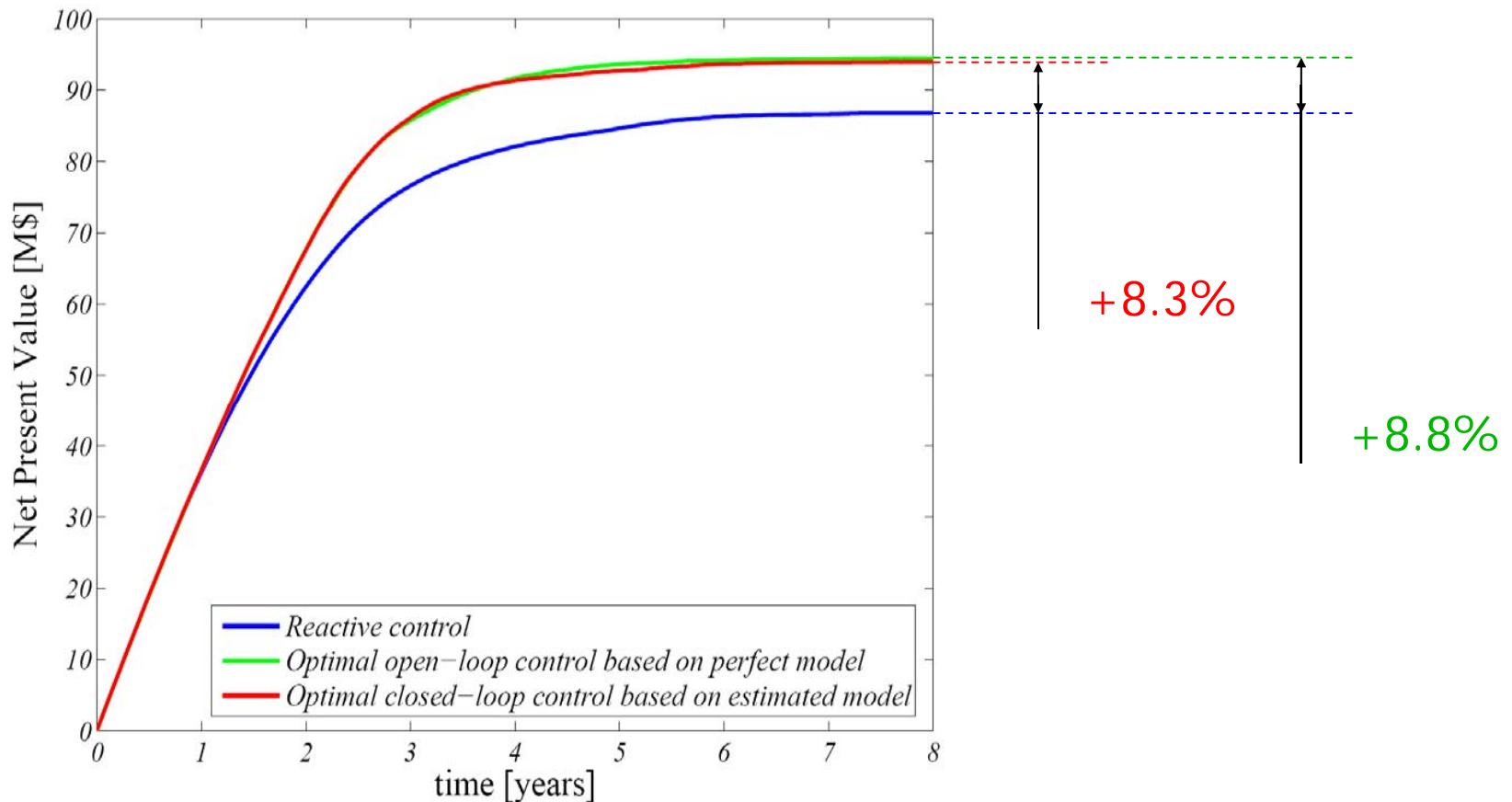
- As prior information an ensemble of initial states $\{\hat{x}_{k|k}\}$ is generated from a given distribution
- By simulating every ensemble member, corresponding ensembles $\{\hat{x}_{k+1|k}\}$ and $\{\hat{y}_{k+1|k}\}$ are generated, and stored as columns of matrices \hat{X} and \hat{Y} respectively
- The measurement update of a EKF is applied to every element of the ensemble, where the covariance matrices are replaced by sampled estimates on the basis of \hat{X} and \hat{Y} .
- The update becomes: $\hat{x}_{k+1|k+1} = \hat{x}_{k+1|k} + K_{k+1}[y_{k+1} - \hat{y}_{k+1|k}]$, where K_{k+1} is given by:
$$K_{k+1} = \hat{X}\hat{Y}^T \cdot [\hat{Y}\hat{Y}^T + R]^{-1} \quad (\text{BLUE})$$
- The result is a new ensemble $\{\hat{x}_{k+1|k+1}\}$

Closed-loop Reservoir Management



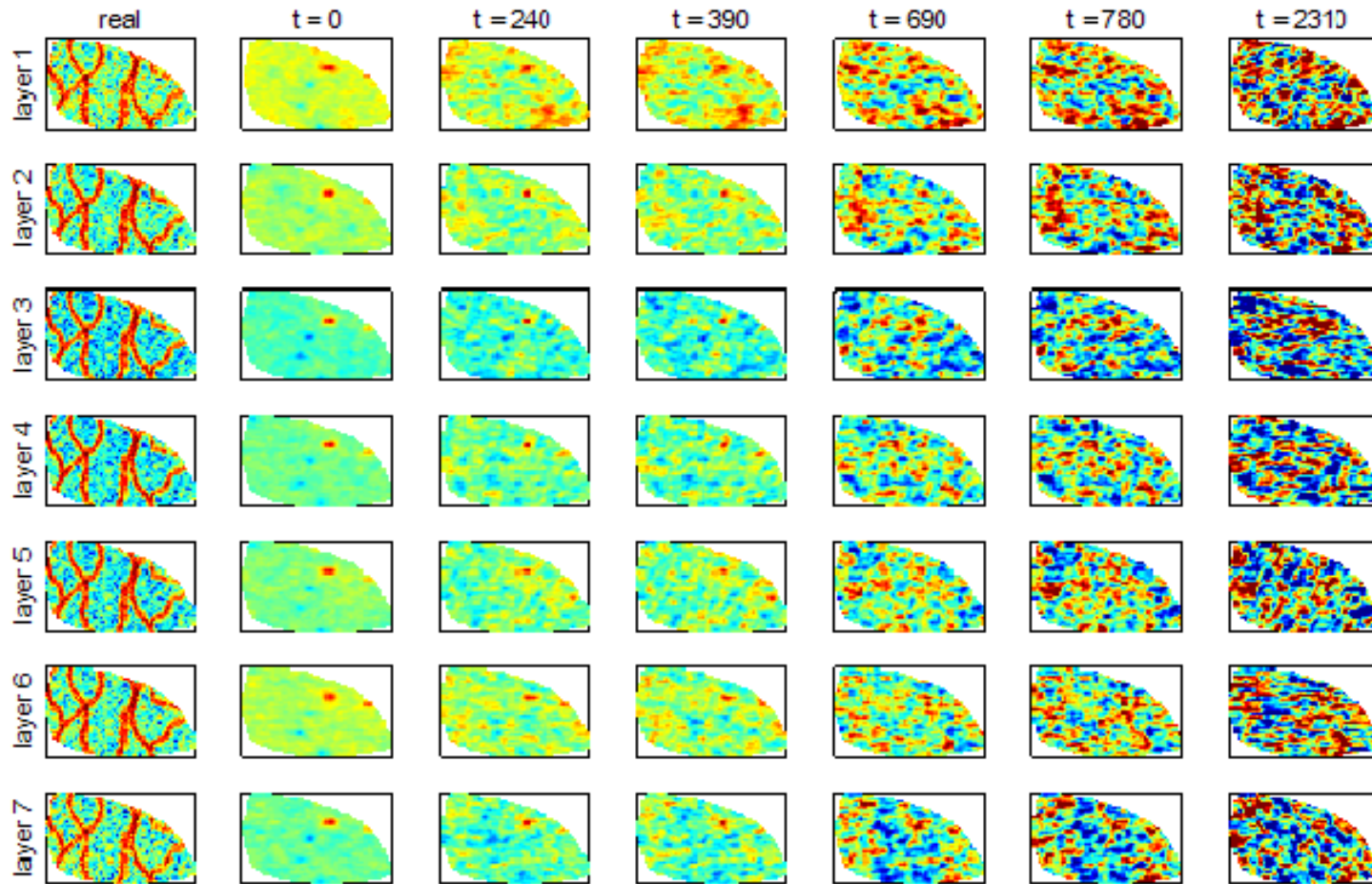
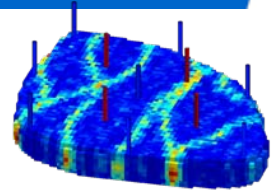
Closed-loop simulation example

- 3 study cases: reactive control, optimal open-loop control based on perfect ('reality') model, optimal closed-loop control

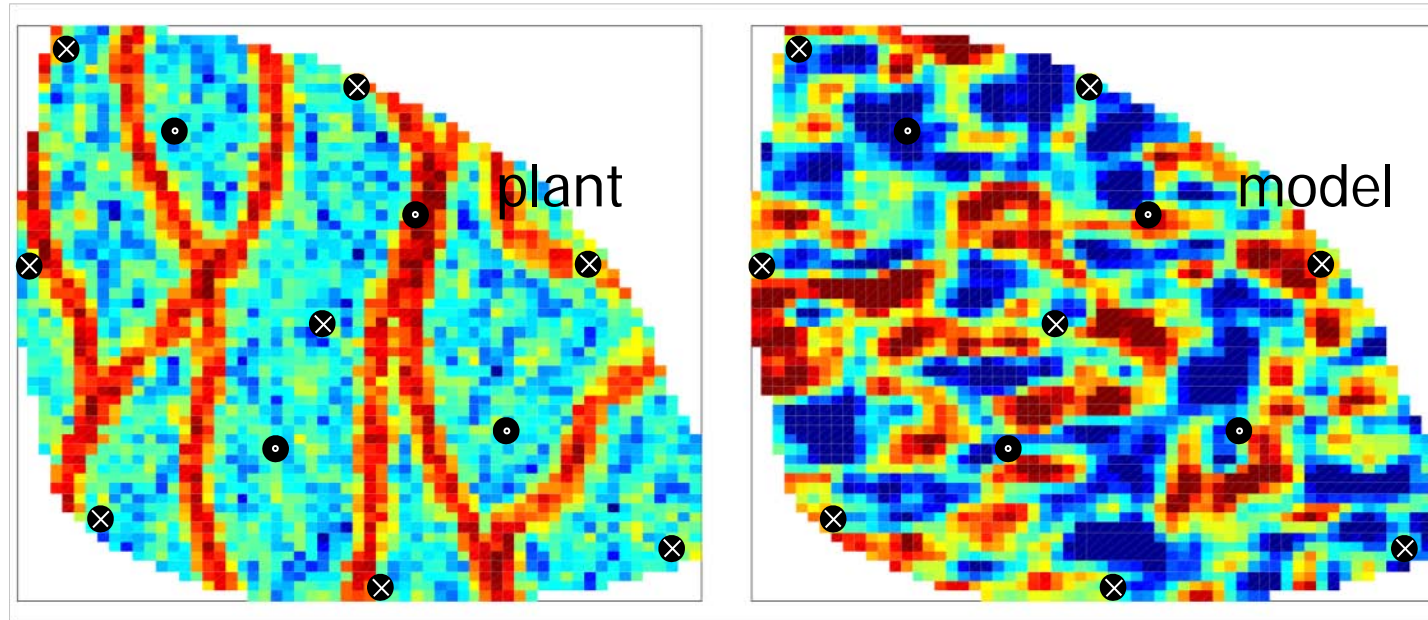


Closed-loop simulation example

Parameter updates at different times



Closed-loop reservoir management



Relatively poor looking models may work quite well!

Limitations and challenges

- Model uncertainty uncertain geology
- Model complexity geological vs control models
- Measurement data limited knowledge
- Nonlinearity dynamics change over lifetime
- Process configuration (dynamic) well placement

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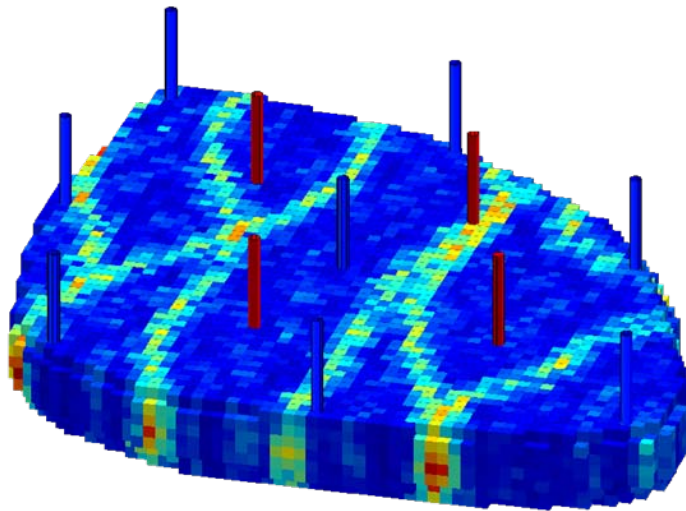
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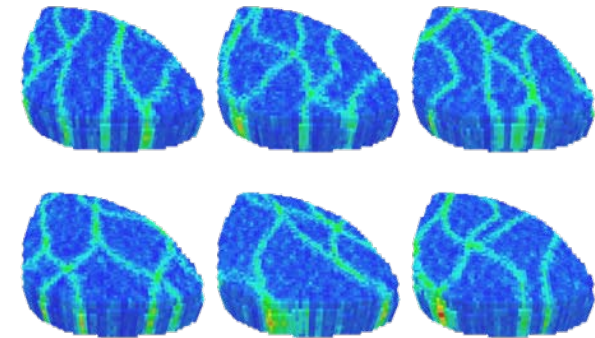
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Robust optimization

- Reservoir models / permeability structure are highly uncertain



model realizations



- Use 100 realizations in a max-mean approach:

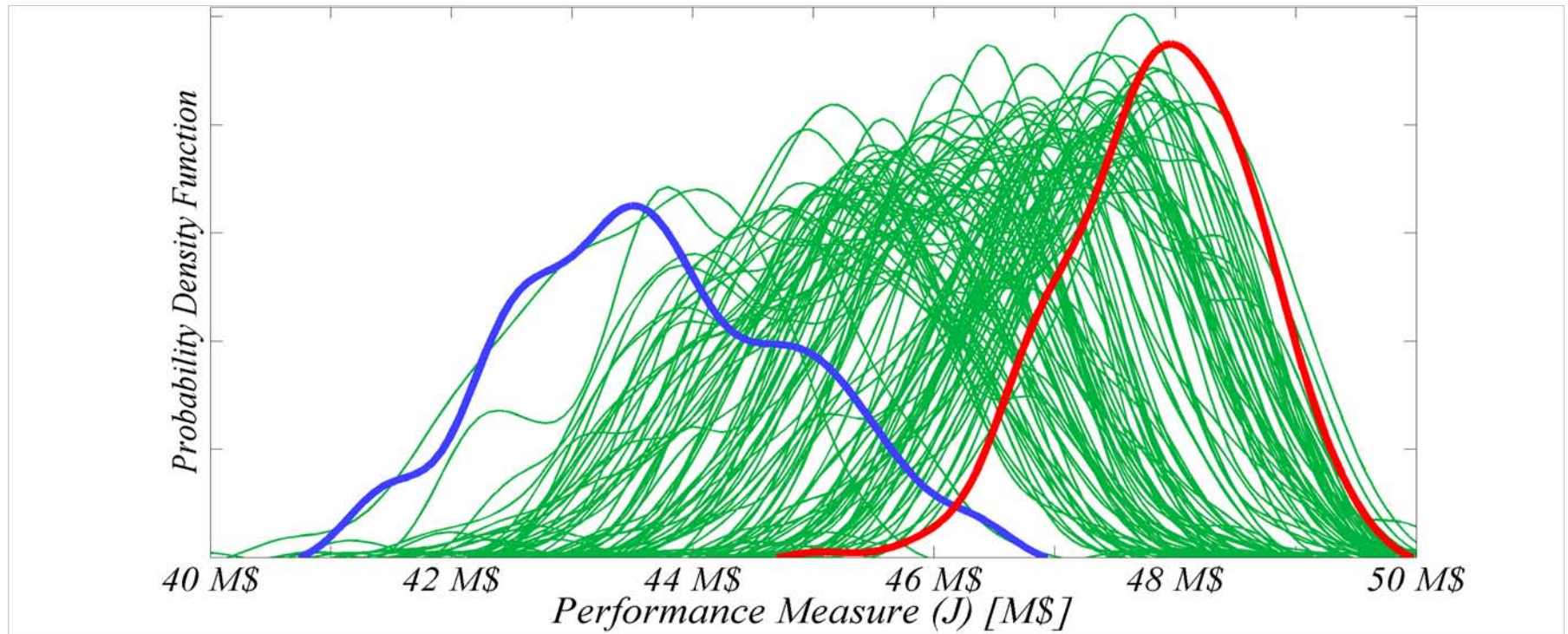
$$\max_{\mathbf{u}} \left(\frac{1}{M} \sum_{i=1}^M J_K(\mathbf{u}, \theta_i) \right)$$

[Gijs van Essen et al., Proc. CCA, 2006]

Robust optimization example

3 control strategies applied to set of 100 realizations:

- reactive control, nominal optimization (100 strategies), robust optimization

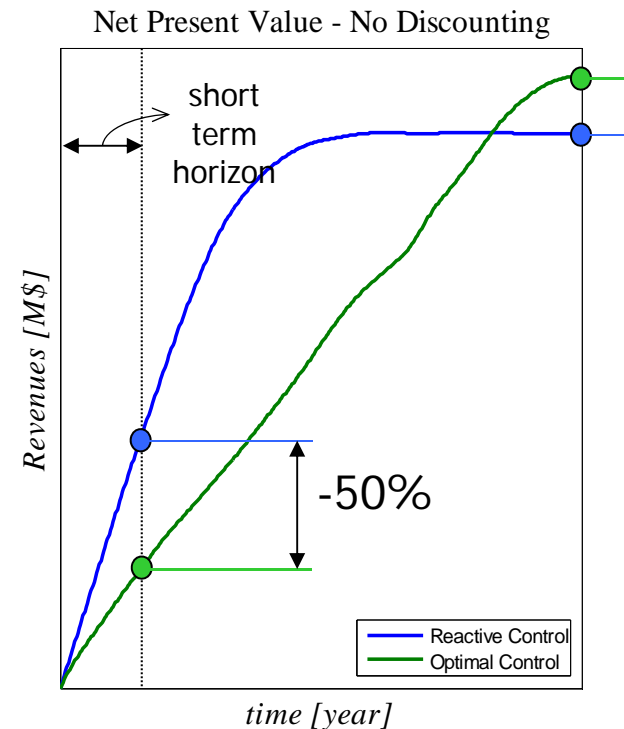
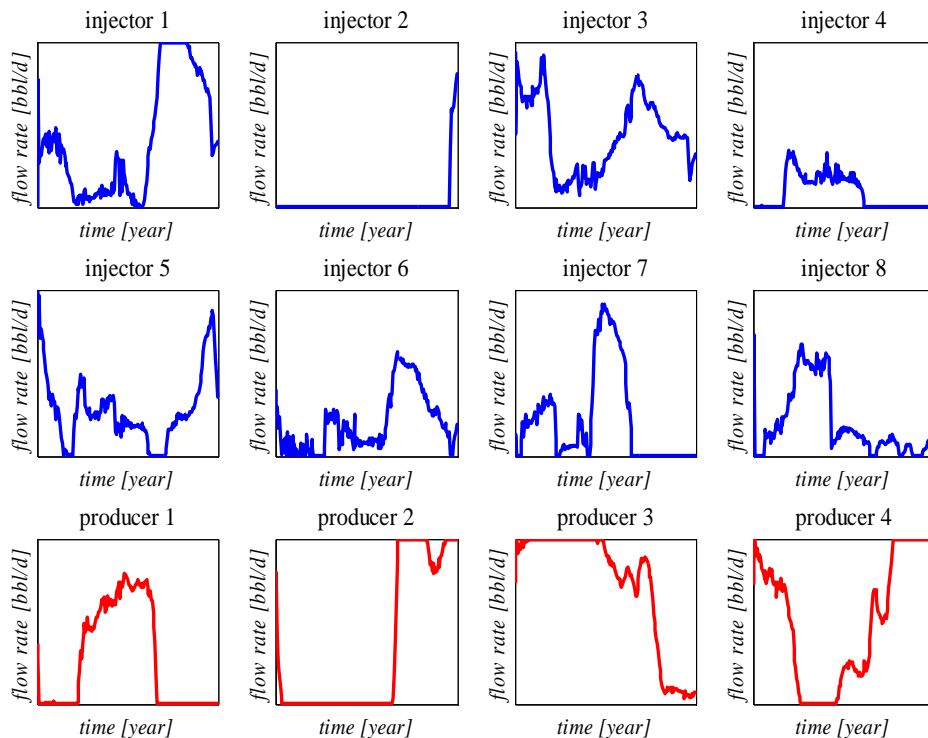


[Van Essen et al, SPE J, 2009]

(each strategy is applied to 100 "systems")

Hierarchical optimization

- Focussing on life-time (long-term) NPV has limitations:
 - Compromise in short-term production
 - Erratic operational strategy



[Van Essen et al, SPE J, 2009]

Hierarchical optimization

- Distinguish two different objective functions:

$$\mathbf{u}^* = \arg \max_{\mathbf{u}} J_K^{(1)}(\mathbf{u}, x_0)$$

with $J_K^{(1)}$ the **long-term NPV**

- Additionally optimize for short-term production:

$$\tilde{\mathbf{u}}^* = \arg \max_{\mathbf{u}} J_K^{(2)}(\mathbf{u}, x_0)$$

such that $J_K^{(1)}(\mathbf{u}, x_0) \geq J_K^{(1)}(\mathbf{u}^*, x_0) - \varepsilon$

with $J_K^{(2)}$ the **short-term NPV**

Utilize degrees of freedom in the input to optimize short-term production

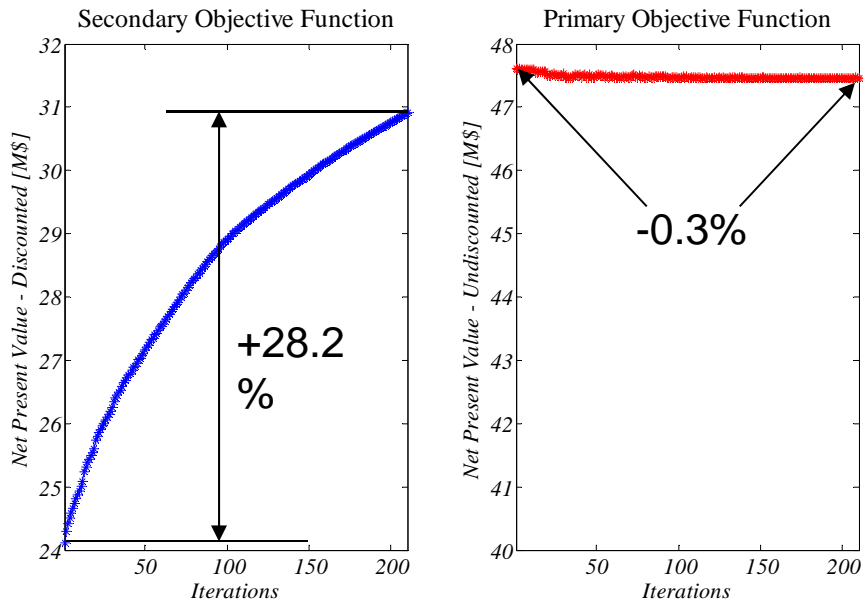
[Van Essen et al, SPE J, 2011]

Objective function with ridges

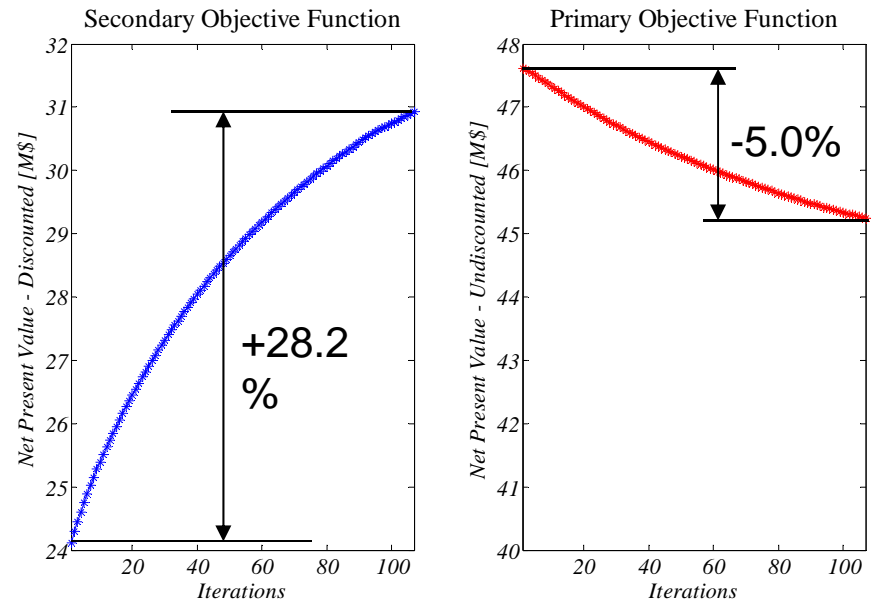


Hierarchical optimization example

Optimization of secondary objective function - constrained to null-space of primary objective

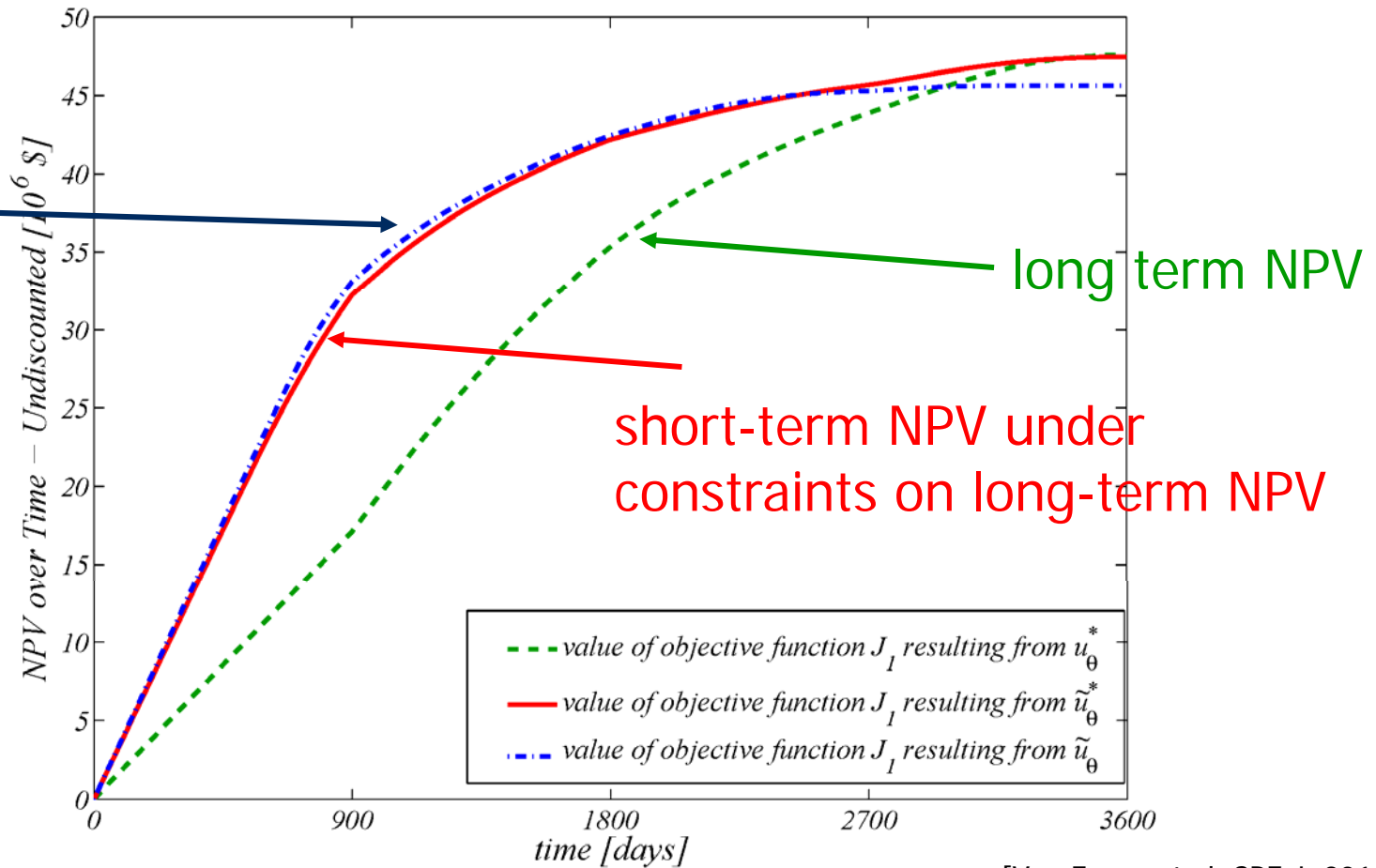


Optimization of secondary objective function - unconstrained



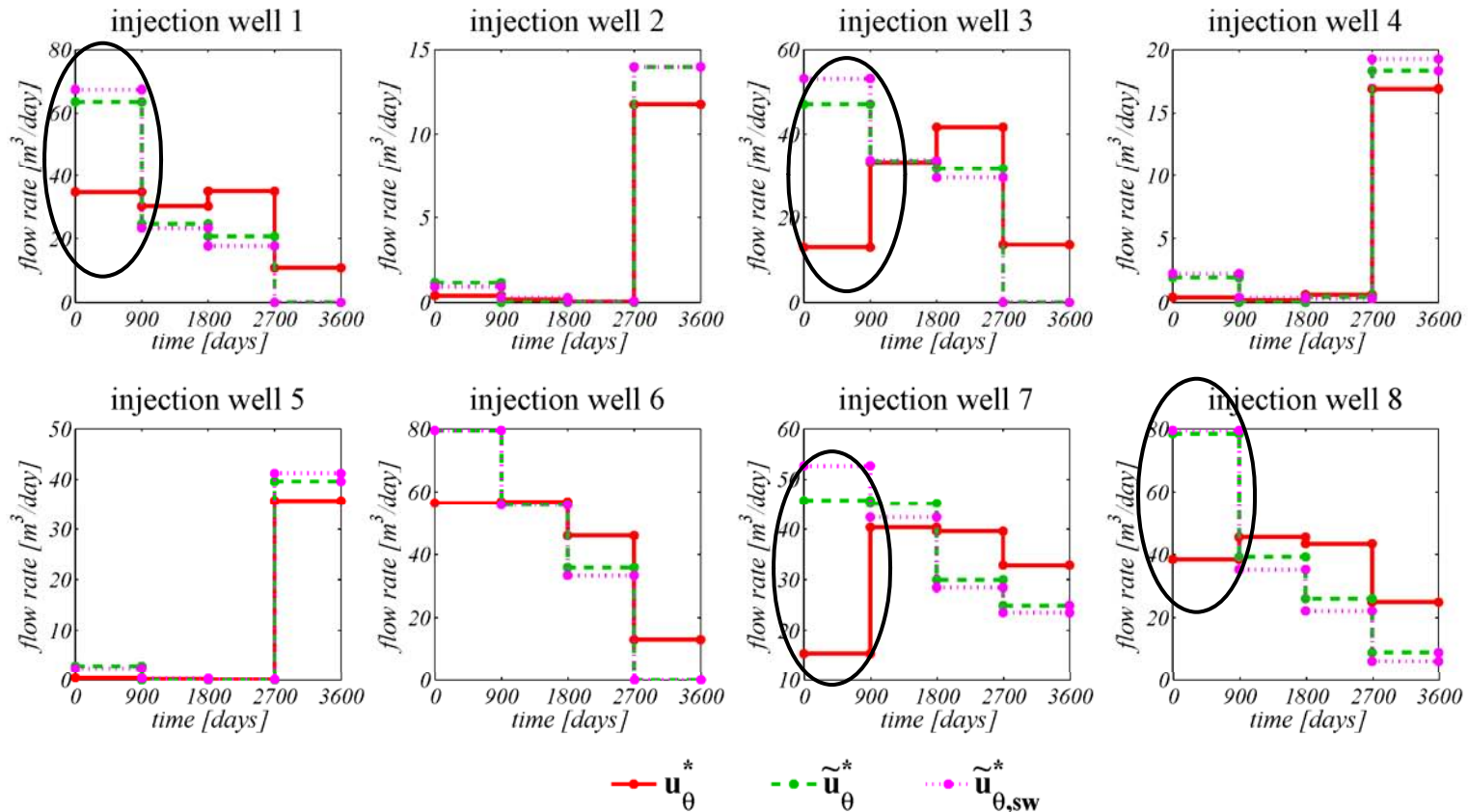
Hierarchical optimization example

Short-term
NPV



[Van Essen et al, SPE J, 2011]

Hierarchical optimization example



Long-term optimized

Short-term constrained optimized

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Parameter Estimation

Typical approach in geological models:

- Use EnKF to estimate states
- Consider parameters (grid-block permeabilities) as extended states
- Estimate **parameters and states**, based on an initial ensemble
 - Data not sufficiently informative to estimate all parameters
 - Parameters are updated only in directions where data contains information

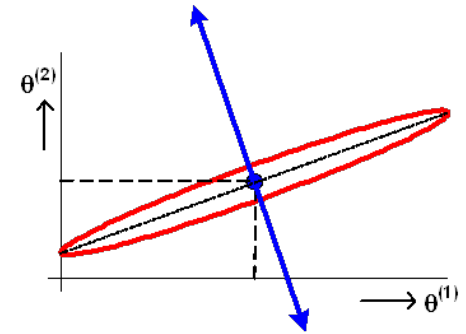
Result and reliability is crucially dependent on initial state/model

Parameter Estimation

Bayesian approach:

$$V_p(\theta) := V(\theta) + \frac{1}{2}(\theta - \theta_p)P_{\theta_p}^{-1}(\theta - \theta_p)$$

The equation is annotated with a red circle around $V(\theta)$ and a red arrow pointing to the word "data". The second term is enclosed in a blue oval with a blue arrow pointing to the word "priors".



Lack of identifiability: Hessian of V is poorly conditioned

- The Bayesian estimate becomes heavily determined by priors

Parametrization can be reduced by projecting unto the (locally) identifiable subspace [Van Doren et al, IFAC 2008,2011]

Several alternatives for reduction of parameter space

[Durlovsky et al., 1996; Zhang et al. 2008; Van Doren, 2010; Jafarpour & McLaughlin, 2008,2009; Tavakoli & Reynolds, 2010]

Capturing long-term behaviour (nonlinear) is the challenge

Testing local identifiability in model estimation

- Consider quadratic identification criterion based on prediction errors

$$V(\boldsymbol{\theta}) := \frac{1}{2} \boldsymbol{\epsilon}(\boldsymbol{\theta})^T \mathbf{P}_v^{-1} \boldsymbol{\epsilon}(\boldsymbol{\theta}), \quad \boldsymbol{\epsilon}(\boldsymbol{\theta}) = \mathbf{y} - \hat{\mathbf{y}} = \mathbf{y} - \mathbf{h}(\boldsymbol{\theta}, \mathbf{u}; \mathbf{x}_0),$$

- Hessian given by

$$\frac{\partial^2 V(\boldsymbol{\theta})}{\partial \boldsymbol{\theta}^2} = \frac{\partial \hat{\mathbf{y}}^T}{\partial \boldsymbol{\theta}} \mathbf{P}_v^{-1} \left(\frac{\partial \hat{\mathbf{y}}^T}{\partial \boldsymbol{\theta}} \right)^T + \mathbf{S}$$

- Local identifiability test in $\hat{\boldsymbol{\theta}} = \arg \min V(\boldsymbol{\theta})$: Hessian > 0

- With quadratic approximation of cost function around $\hat{\boldsymbol{\theta}}$:

Hessian given by

$$\frac{\partial \hat{\mathbf{y}}^T}{\partial \boldsymbol{\theta}} \mathbf{P}_v^{-1} \left(\frac{\partial \hat{\mathbf{y}}^T}{\partial \boldsymbol{\theta}} \right)^T$$

Testing local identifiability in identification

- Rank test on Hessian through SVD

$$\left. \frac{\partial \hat{\mathbf{y}}^T}{\partial \boldsymbol{\theta}} \mathbf{P}_v^{-\frac{1}{2}} \right|_{\boldsymbol{\theta}=\hat{\boldsymbol{\theta}}} = \begin{bmatrix} \mathbf{U}_1 & \mathbf{U}_2 \end{bmatrix} \begin{bmatrix} \boldsymbol{\Sigma}_1 & \mathbf{0} \\ \mathbf{0} & \boldsymbol{\Sigma}_2 \end{bmatrix} \begin{bmatrix} \mathbf{V}_1^T \\ \mathbf{V}_2^T \end{bmatrix}$$

- If $\boldsymbol{\Sigma}_2 = \mathbf{0}$ then lack of local identifiability
- SVD can be used to reparameterize the model structure through

$$\boldsymbol{\theta} = \mathbf{U}_1 \boldsymbol{\rho}, \quad \dim(\boldsymbol{\rho}) \ll \dim(\boldsymbol{\theta})$$

in order to achieve local identifiability in $\boldsymbol{\rho}$

- Columns of \mathbf{U}_1 are basis functions of the identifiable parameter space

Testing local identifiability in identification

$$\left. \frac{\partial \hat{\mathbf{y}}^T}{\partial \boldsymbol{\theta}} \mathbf{P}_v^{-\frac{1}{2}} \right|_{\boldsymbol{\theta}=\hat{\boldsymbol{\theta}}} = \begin{bmatrix} \mathbf{U}_1 & \mathbf{U}_2 \end{bmatrix} \begin{bmatrix} \boldsymbol{\Sigma}_1 & \mathbf{0} \\ \mathbf{0} & \boldsymbol{\Sigma}_2 \end{bmatrix} \begin{bmatrix} \mathbf{V}_1^T \\ \mathbf{V}_2^T \end{bmatrix}$$

- What if $\boldsymbol{\Sigma}_2 \neq \mathbf{0}$ but contains (many) small singular values ?

No lack of identifiability, but possibly very poor variance properties

- Identifiability mostly considered in a yes/no setting: qualitative rather than quantitative [Bellman and Åström (1970), Grewal and Glover (1976)]
- Approach: *quantitative* analysis of appropriate parameter space, maintaining physical parameter interpretation

Approximating the identifiable parameter space

Asymptotic variance analysis: $\text{cov}(\hat{\boldsymbol{\theta}}) = J^{-1} = \left(\mathbb{E} \left[\frac{\partial^2 V(\boldsymbol{\theta})}{\partial \boldsymbol{\theta}^2} \middle| \hat{\boldsymbol{\theta}} \right] \right)^{-1}$

with $J =$ Fisher Information Matrix.

- Sample estimate of parameter variance, on the basis of $V(\boldsymbol{\theta})$:

$$\text{cov}(\hat{\boldsymbol{\theta}}) = \begin{cases} \begin{bmatrix} \mathbf{U}_1 & \mathbf{U}_2 \end{bmatrix} \begin{bmatrix} \boldsymbol{\Sigma}_1^{-2} & \mathbf{0} \\ \mathbf{0} & \boldsymbol{\Sigma}_2^{-2} \end{bmatrix} \begin{bmatrix} \mathbf{V}_1^T \\ \mathbf{V}_2^T \end{bmatrix} & \text{for } \boldsymbol{\Sigma}_2 > 0 \\ \infty & \text{for } \boldsymbol{\Sigma}_2 = 0 \end{cases}$$

$$\text{cov}(\mathbf{U}_1 \hat{\boldsymbol{\rho}}) = \mathbf{U}_1 \boldsymbol{\Sigma}_1^{-2} \mathbf{U}_1^T$$

$$\text{cov}(\hat{\boldsymbol{\theta}}) > \text{cov}(\mathbf{U}_1 \hat{\boldsymbol{\rho}}) \quad \text{if } \boldsymbol{\Sigma}_2 > 0$$

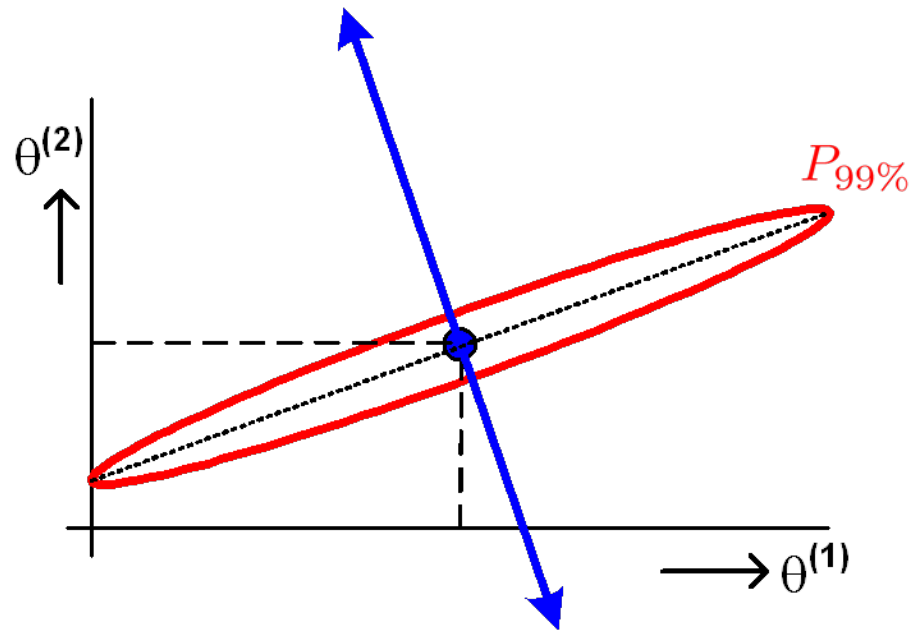
Approximating the identifiable parameter space

$$\text{cov}(\hat{\boldsymbol{\theta}}) > \text{cov}(\mathbf{U}_1 \hat{\boldsymbol{\rho}}) \quad \text{if } \boldsymbol{\Sigma}_2 > 0$$

- Discarding singular values that are small, reduces the variance of the resulting parameter estimate
- Particularly important in situations of (very) large numbers of small s.v.'s
- Model structure approximation (local)
- Quantified notion of identifiability – related to parameter variance

Approximating the identifiable parameter space

- Interpretation:
Remove the parameter directions that are poorly identifiable (have large variance)

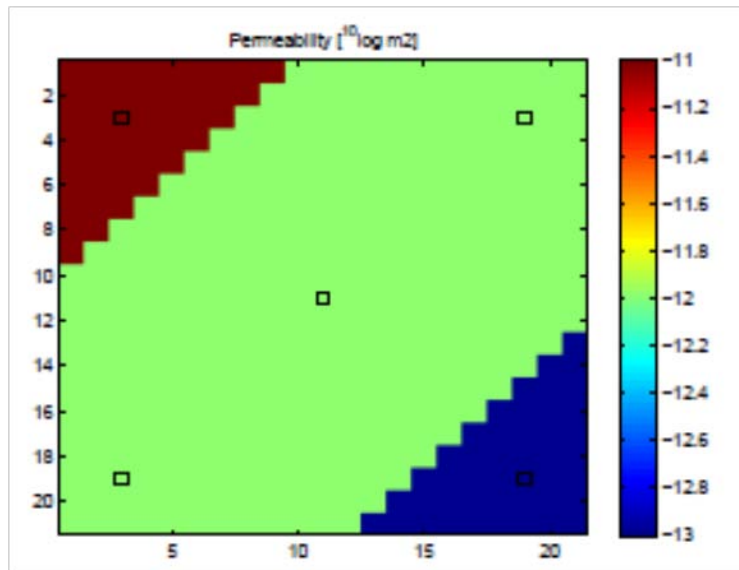


- This is different from removing the (separate) parameters for which the value 0 lies within the confidence bound [Hjalmarsson, 2005]

Simple reservoir example

[Van Doren, 2010]

2D two-phase example
(top view)



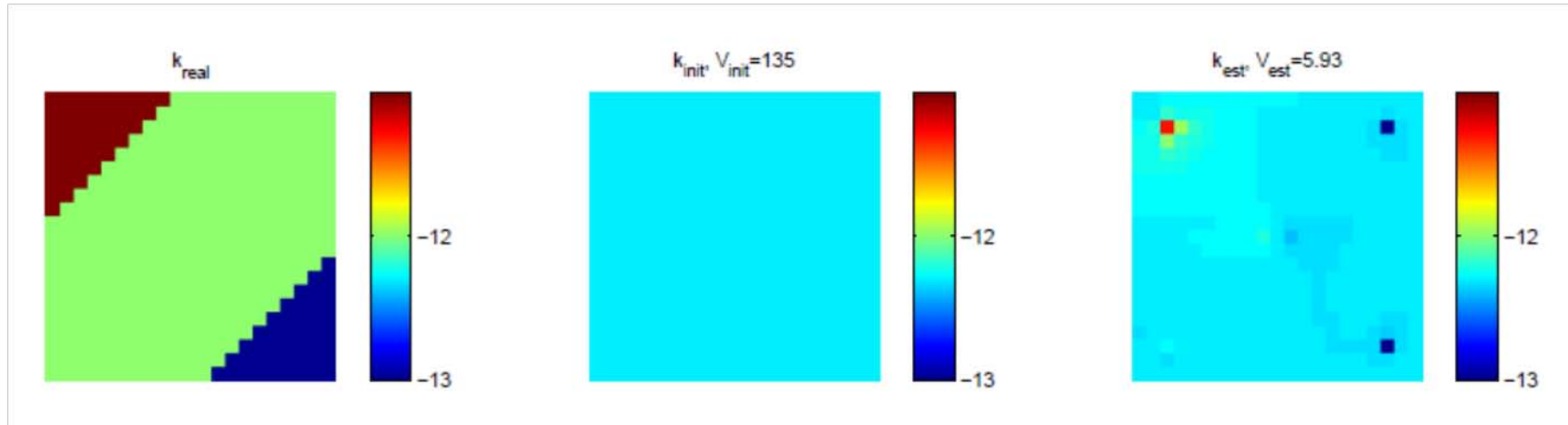
21 x 21 grid block permeabilities
5 wells; 3 permeability strokes

1 injector (centre)
4 producers (corners)

5 inputs: 1 injector flow-rate, and 4 bottom hole pressures
8 outputs: producer flow rates (water and oil)

Simple reservoir example

Using the reduced parameter space –iteratively- in estimation:



exact field

initial estimate
(local point)

final estimate

Observation:

Only grid block permeabilites around well are identifiable.

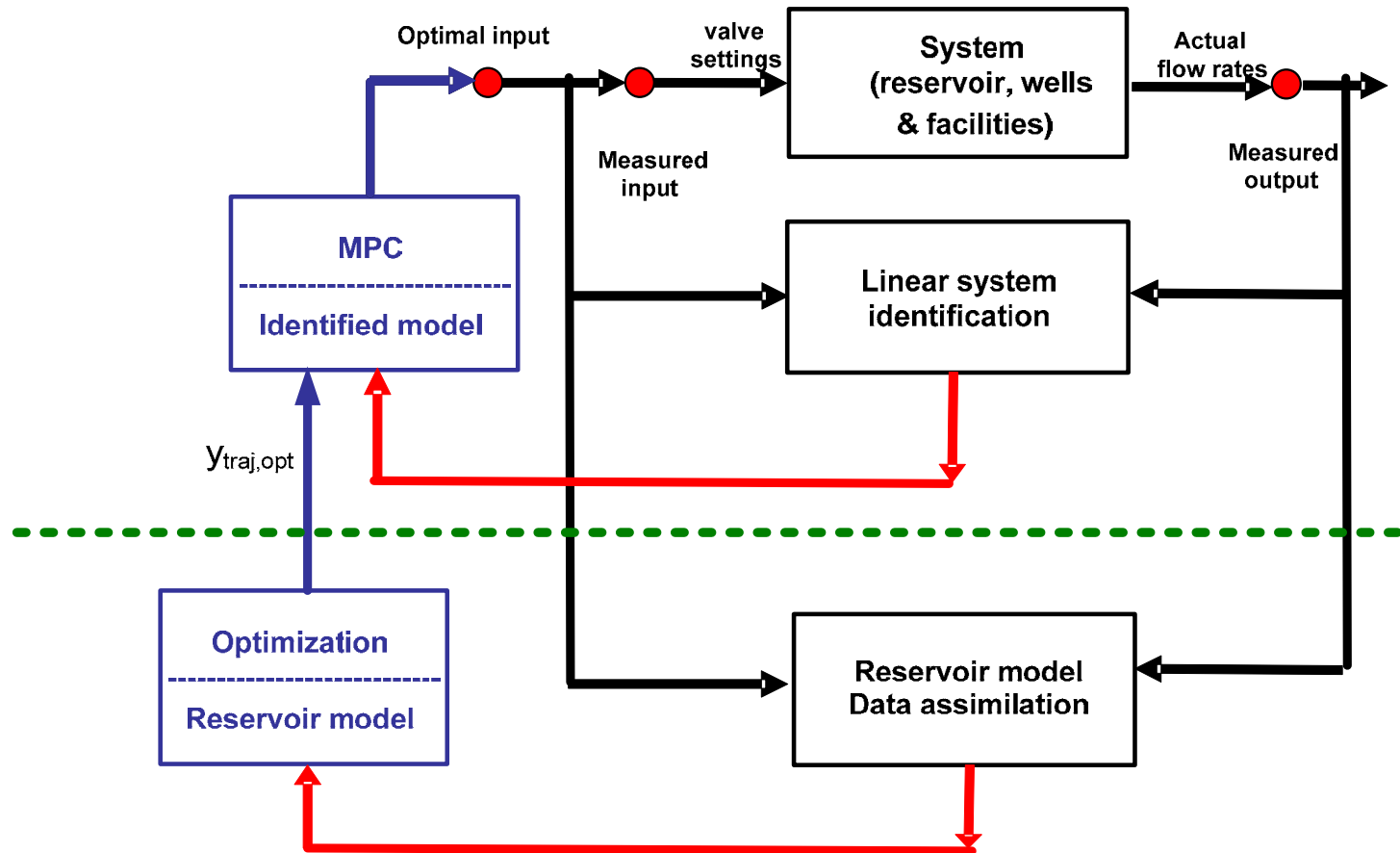
Time-scale separation – Two-level approach

Reasoning

- Optimization on the basis of **nonlinear reservoir models** suffers from model uncertainties
- Optimization on the basis of **identified (linear) models** suffers from a lack of predictive capabilities beyond the –local– measurement interval

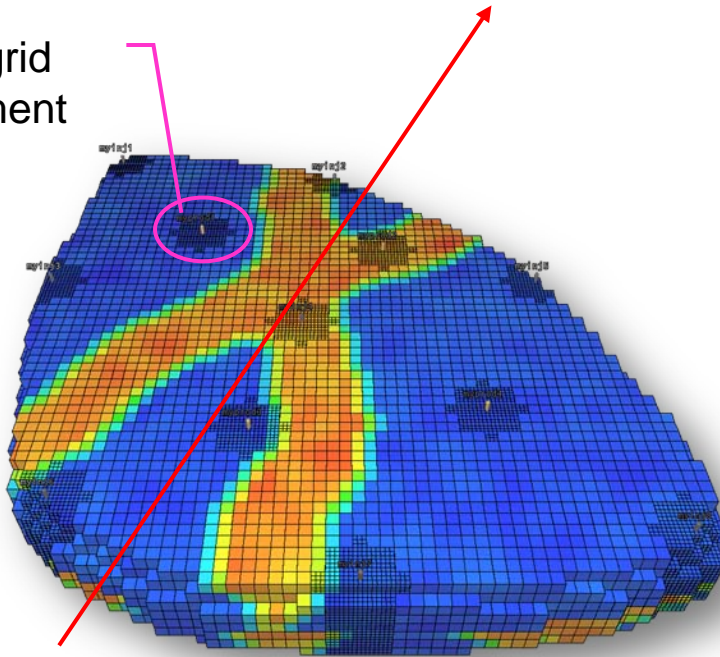
 **Combine the two**

Two-level approach



Example: 3D reservoir

local grid refinement

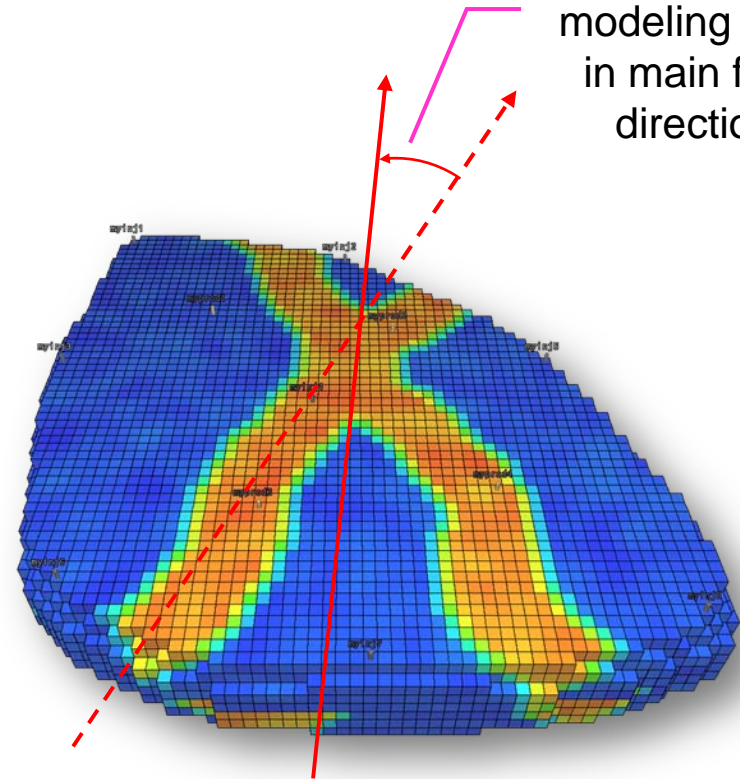


'truth' model

time step size: 0.25 days

8 injection wells, 4 production wells

modeling error in main flow direction



reservoir model

time step size: 30 days

Modeling error due to geological uncertainty & undermodeling of fast, local dynamics

Example: 3D reservoir

3 production strategies

1. Reactive control

- Maximal injection rates/minimal bottom-hole pressures
- Shut-in wells when watercut >0.90

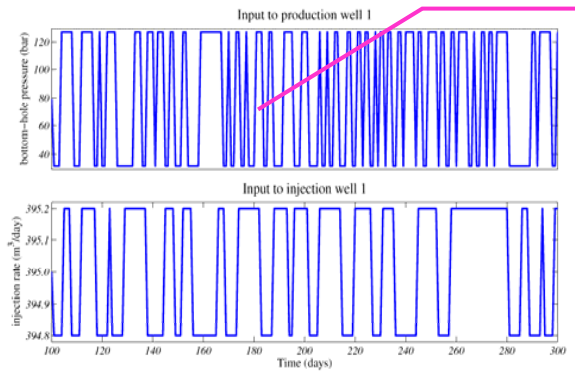
2. Open-loop life-cycle optimization

- Optimize inputs based on reservoir model
- Apply to 'truth' model

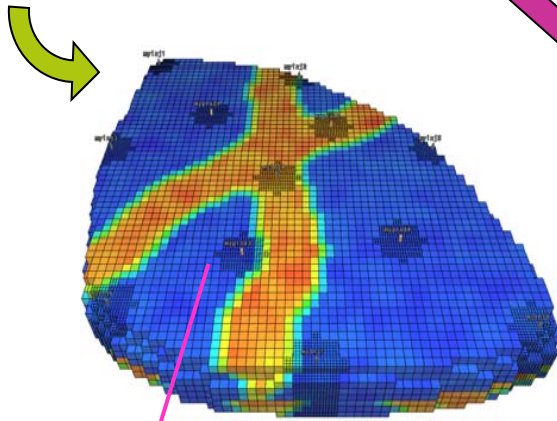
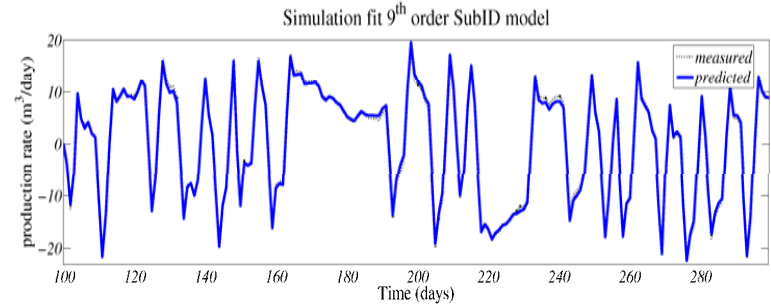
3. Combined dynamic optimization & MPC control

- Life-cycle optimization on reservoir model to obtain references
- Excitation on 'truth' model to identify low-order model
- MPC on 'truth' model to track references

Low-order linear modeling (system id)

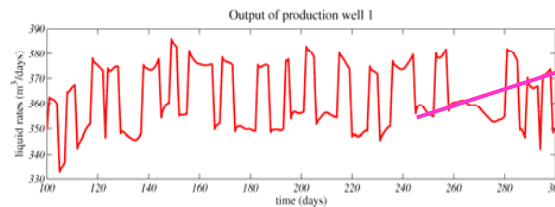


Persistently
exciting inputs
=
Injection rates
&
Producer BHP's



System
Identification

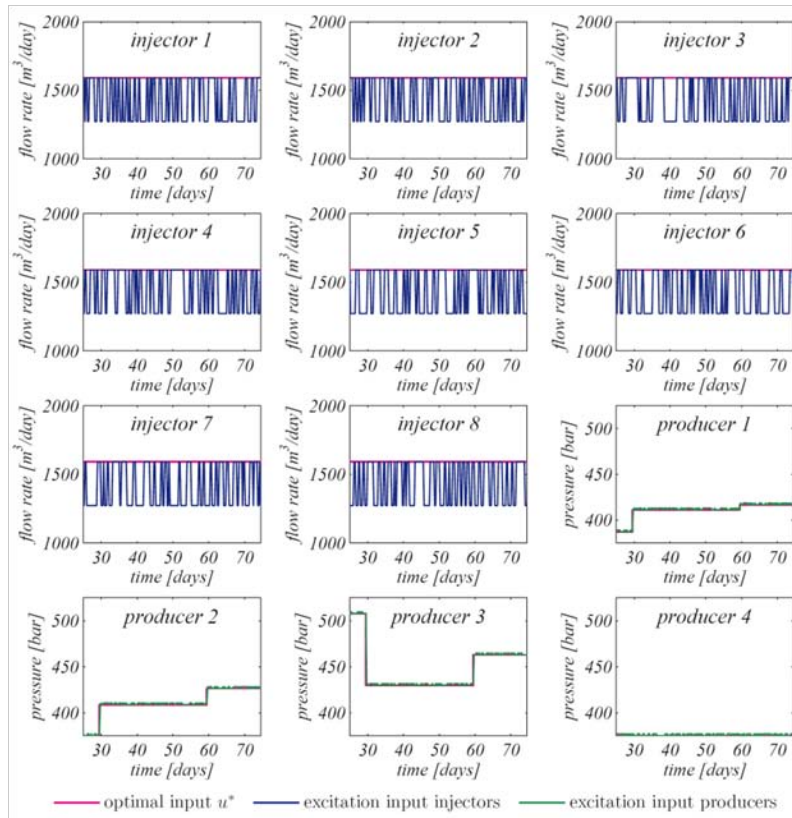
identified
model



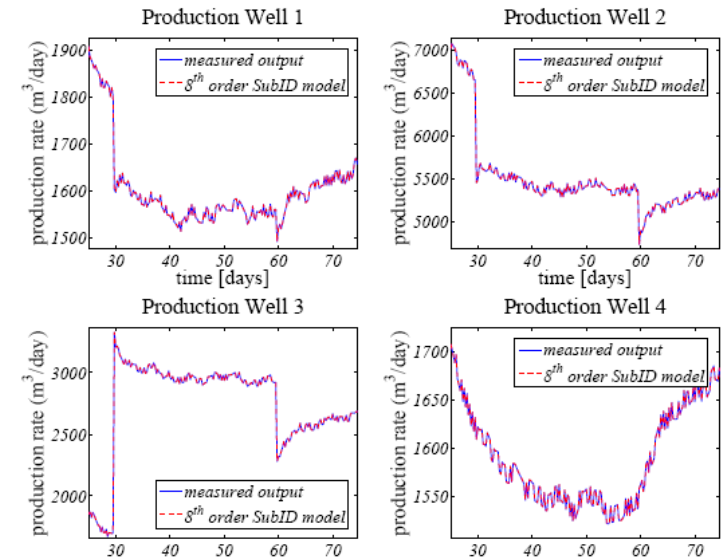
Liquid
production flow
rates

Example: Identification Experiment

Input excitation for identification



sub-space
identification



Simulation fit of 8th
order identified model

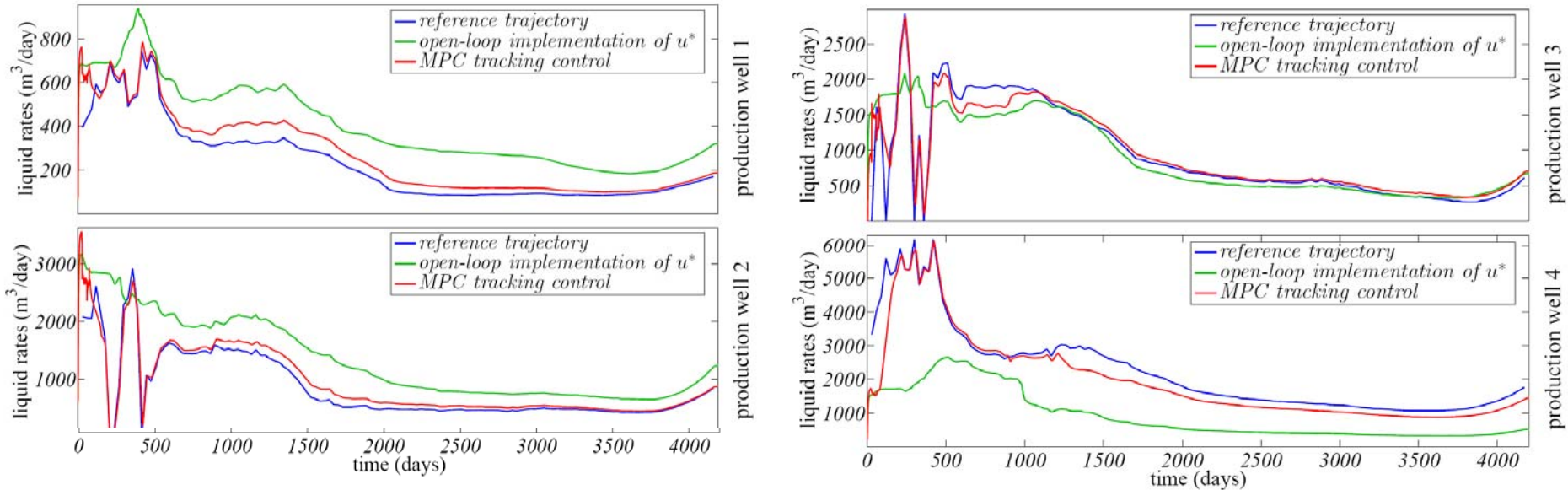
Example: Results

	<i>NPV</i>	<i>%</i>
<i>Case 1: Reactive Control</i>	550 M\$	-
<i>Case 2: Open-loop Optimization</i>	558 M\$	+1.5%
<i>Case 3: Two-level Control</i>	594 M\$	+8.0%
<i>Maximum based on reservoir model</i>	596 M\$	+8.4%

[Van Essen et al., CDC 2010]

Example: Results

Production rates at the 4 producers



Optimized model output traj

Designed input applied to plant

MPC tracking controlled plant

Control relevant models

- What are the important physical phenomena in the reservoir that are essential for the optimized operational strategy?
- There is a serious gap between the reservoir models with geological relevance, and goal-oriented models that are fit for control/optimization.

Summary

- Challenging problems in model-based operation on the basis of highly uncertain information
- Systems and control tools play an important role
- Size of the prize: field tests

- Key elements:
 - **Model-based optimization** under physical constraints and geological **uncertainties**
 - Appropriate merging of **physical and measured data** in **low-order** reliable and **goal-oriented models**
 - Capturing the essential **non-linear behaviour** of reservoirs
 - Challenging **parametrization** issues, in relation to control-relevance and **identifiability** (control-relevant geological models?)
 - **Learning** the optimal strategy in one shot (batch)

The Team:

Paul Van den Hof



Gijs van Essen



Jan Dirk Jansen



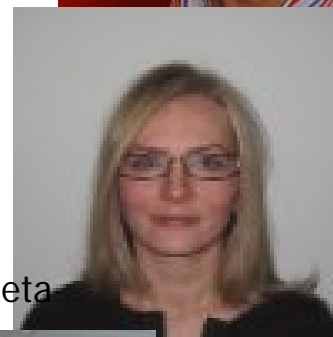
Arnold Heemink



Okko Bosgra



Malgorzata Kaleta



Mariya Krymskaya



Sippe Douma



Jorn Van Doren



Remus Hanea



Ali Vakili

Further reading

- J.D. Jansen, O.H. Bosgra and P.M.J. Van den Hof (2008).
Journal of Process Control, 18 (9), pp. 846-855.
- P.M.J. Van den Hof, J.D. Jansen and A.W. Heemink (2012).
Plenary paper in:
Proc. 2012 IFAC workshop on Automatic Control in Offshore Oil and Gas Production, NTNU, Norway, pp. 189-200.
(IFAC Papers-on-Line)
- Several control-related papers and thesises available at:
www.dcsc.tudelft.nl/~pvandenhof/publications.htm
or through: p.m.j.vandenhof@tue.nl

Thank you for your attention

Model-Based Optimization and Control of Subsurface Flow in Oil Reservoirs

Paul Van den Hof
with Jan Dirk Jansen, Arnold Heemink

Plenary lecture,
32nd Chinese Control Conference,
26–28 July 2013, Xi'an, China

